

CO₂ EOR

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Recovery factor and EOR

$$RF = \eta_A \times \eta_V \times \eta_\mu$$

Typically:

$\eta_A = 0.8$, dependent on mobility ratio, geology

$\eta_V = 0.8$, dependent on geology, impact of gravity

$\eta_\mu = 0.6$, dependent on process, wettability

EOR is about increasing η_μ

CO₂ EOR

- › CO₂ EOR is mature technology (>30yrs, currently 200 000 bbl/d globally)
- › CO₂ breakthrough between 0.5 and 2 yrs
- › Severe gravity override limits RF
- › Mainly CO₂ from natural sources

No interface

miscible

CO₂ mixing

Low residual oil

CO₂ acts as solvent

immiscible

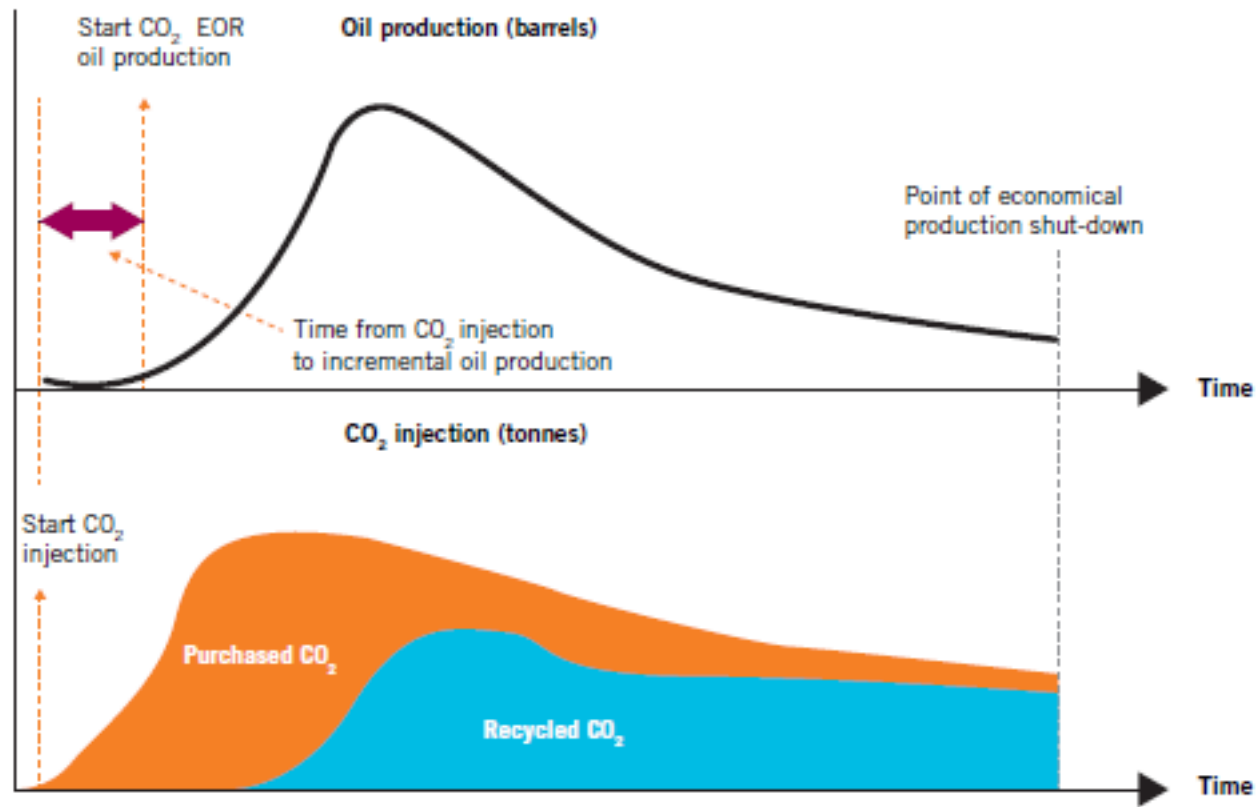
CO₂
dissolved

- Swelling
- Viscosity reduction

Miscible vs Immiscible floods

- › Extra oil 10-15% vs 5-7% for immiscible
- › Consumption 0.4 tCO₂/bbl vs 0.2 tCO₂/bbl immiscible
- › 90% is miscible
- › Massive recirculation
- › WACO₂ is standard approach
- › Largest operations were around 15 000 bbl/d extra oil
- › No primary drives, EOR only

FIGURE 67 The relationship between oil production, purchased CO₂, and recycled CO₂



Source: Jakobsen et al. (2005).

CO₂ EOR economics

- › Extra oil
 - › Miscible 10-15% STOIIP
 - › Immiscible 5-7%

- › CO₂ net consumption
 - › Miscible 0.4 t/bbl
 - › Immiscible 0.2 t/bbl

- › CO₂ purchasing dominates

CO₂ EOR Economics TEXAS

- › Dominated by purchasing costs of CO₂
- › West Texas: CO₂ cost indexed to oil price
assume crude @ 50 \$/bbl -> CO₂ @ 33 \$/t
- › Assume for miscible net consumption: 0.4 t/bbl
CO₂ purchasing cost 14 \$/bbl
- › Assume CAPEX+ OPEX ≈ CO₂ costs
CO₂ EOR miscible UTC: 28 \$/bbl
- › UTC for immiscible estimated 21 \$/bbl @ 50 \$/bbl

Capital Intensive

- › High UTC for CO₂:
- › Smaller companies
- › State oil companies

How CO₂ EOR started



Texas – one pipeline from CO₂ reservoir to one oil field

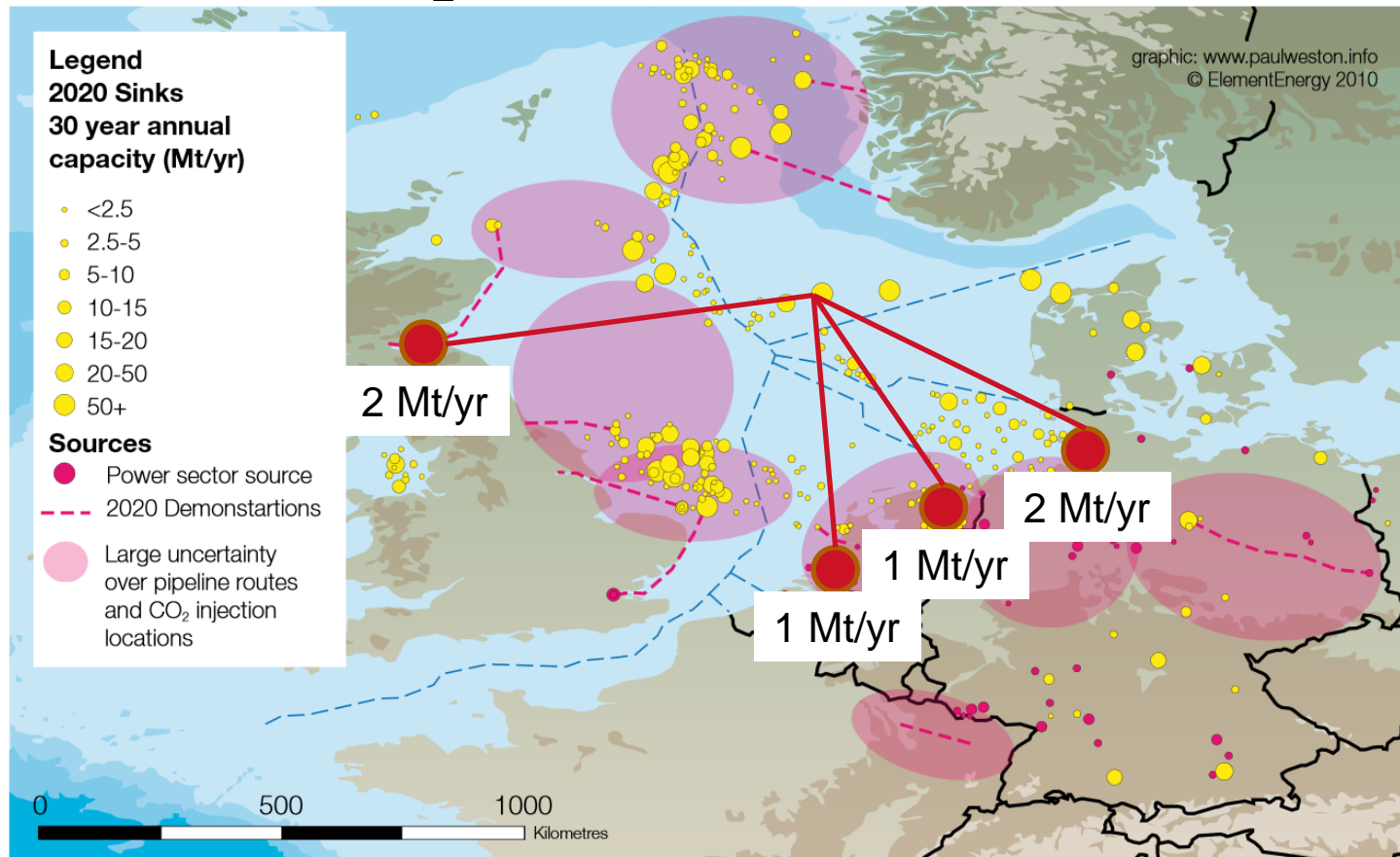
Canada – one pipeline from Beulah (USA) to Weyburn (Canada)

Netherlands – P18-4, Q1, K12B

Coal-fired Power station
Boundary dam
Saskatchewan, Canada



Ship transport *Kick-start CO₂-EOR in North Sea?*



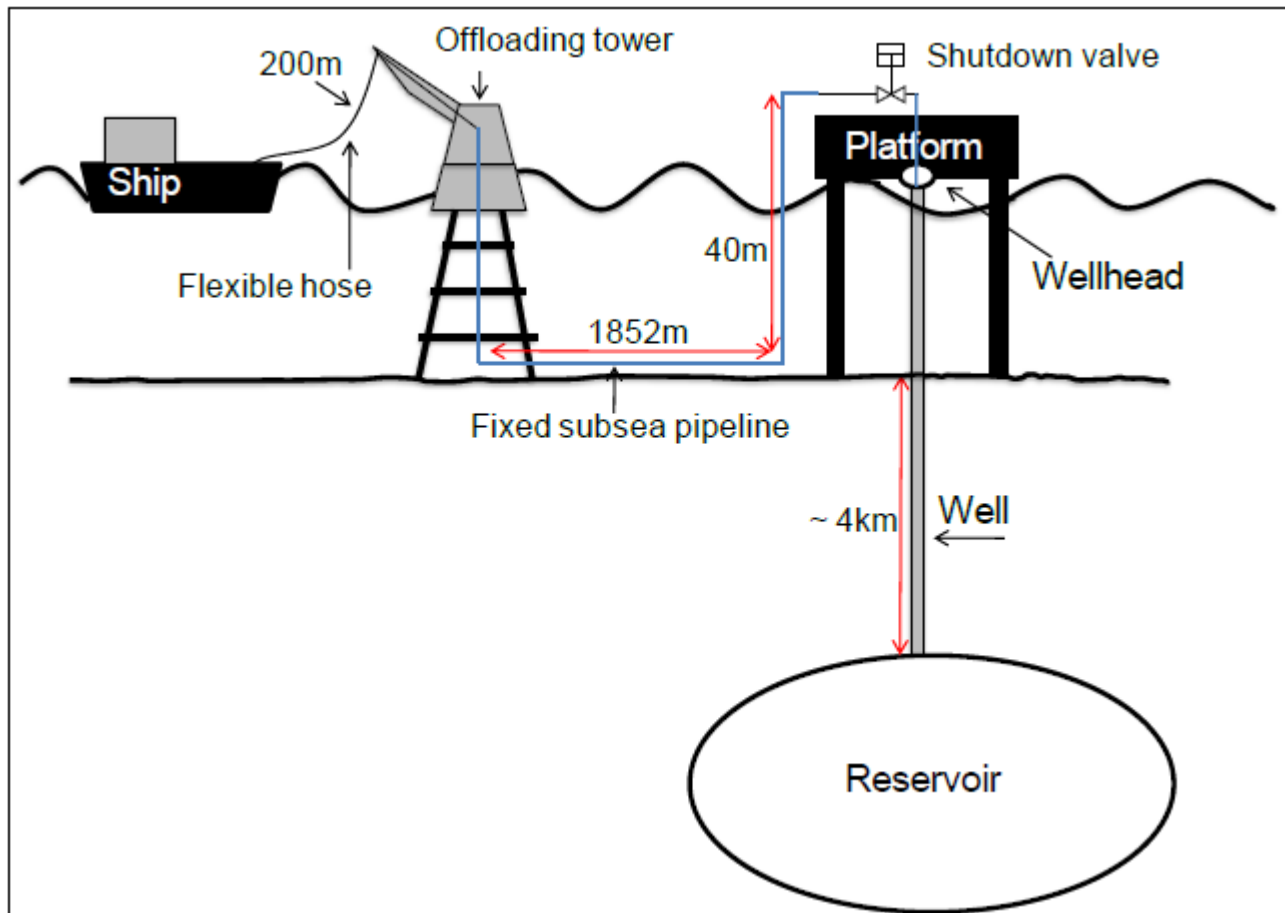
Map: One North Sea, Element Energy, 2010

Proposal for a pilot project: shipping CO₂ to the K12-B reservoir and beyond



Courtesy Anthony Veder

Potential pilot project: shipping CO₂ to the K12-B reservoir



P, T conditions in ship – flowline – reservoir system

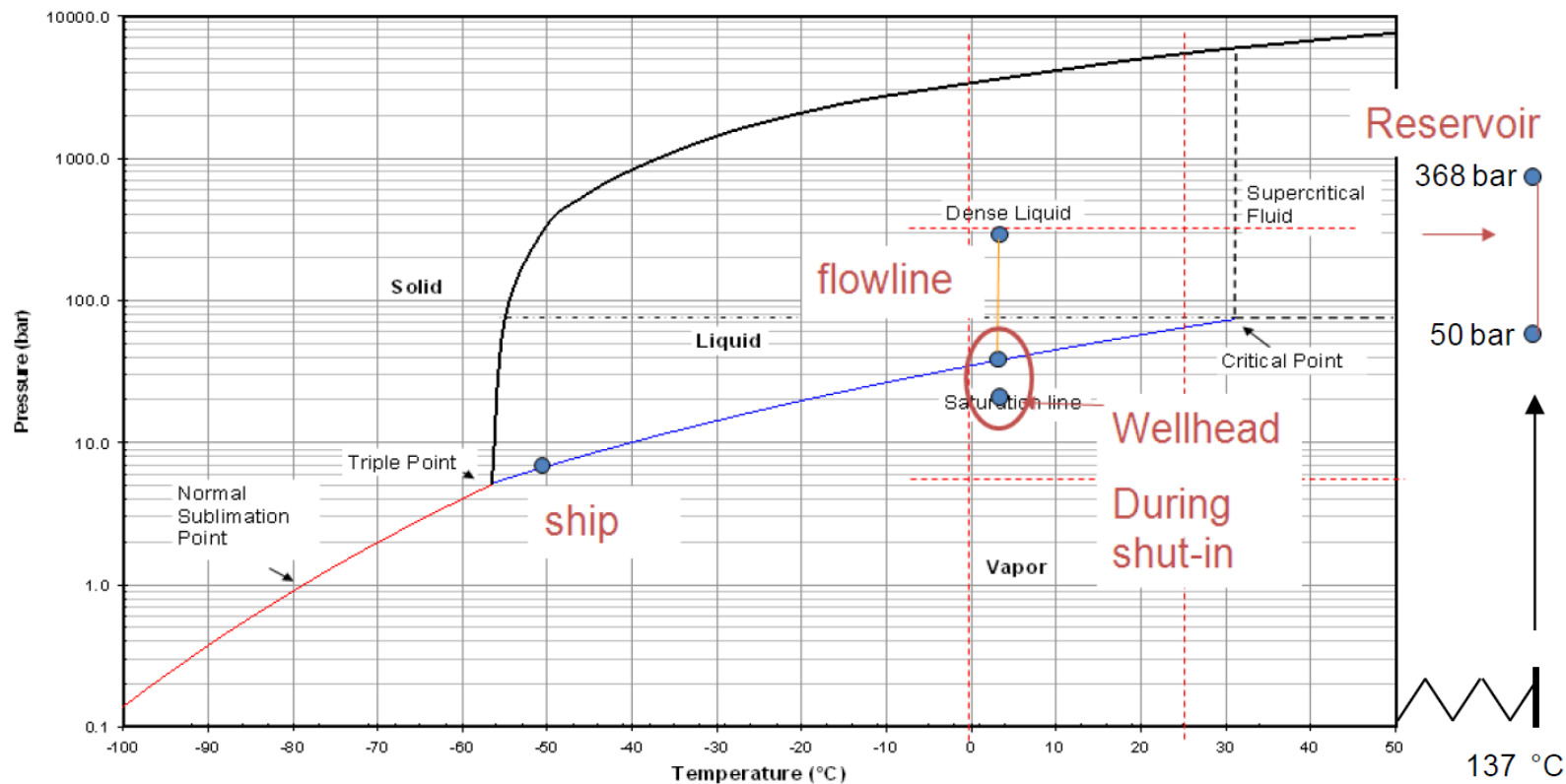
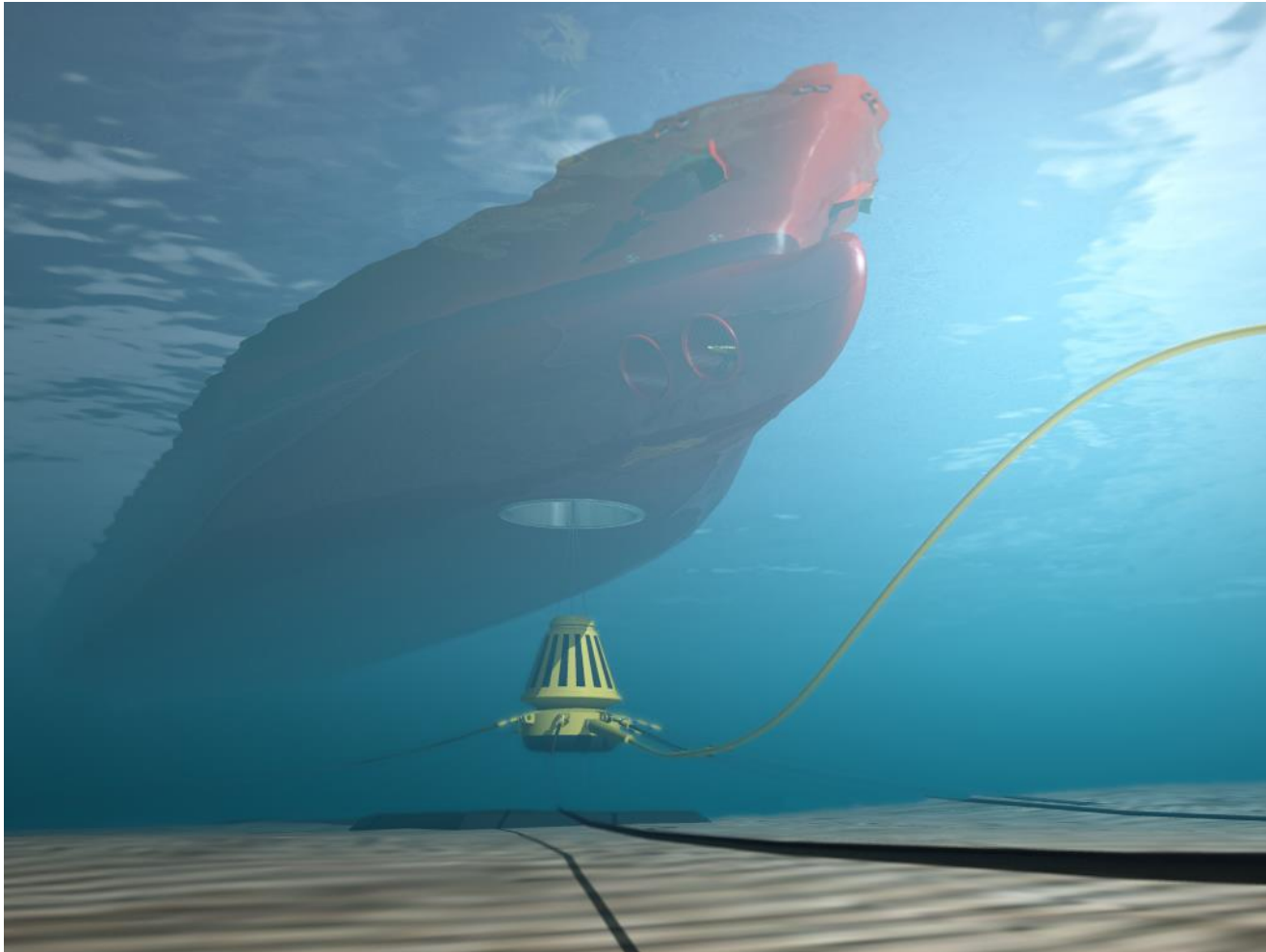


Photo of an offloading tower



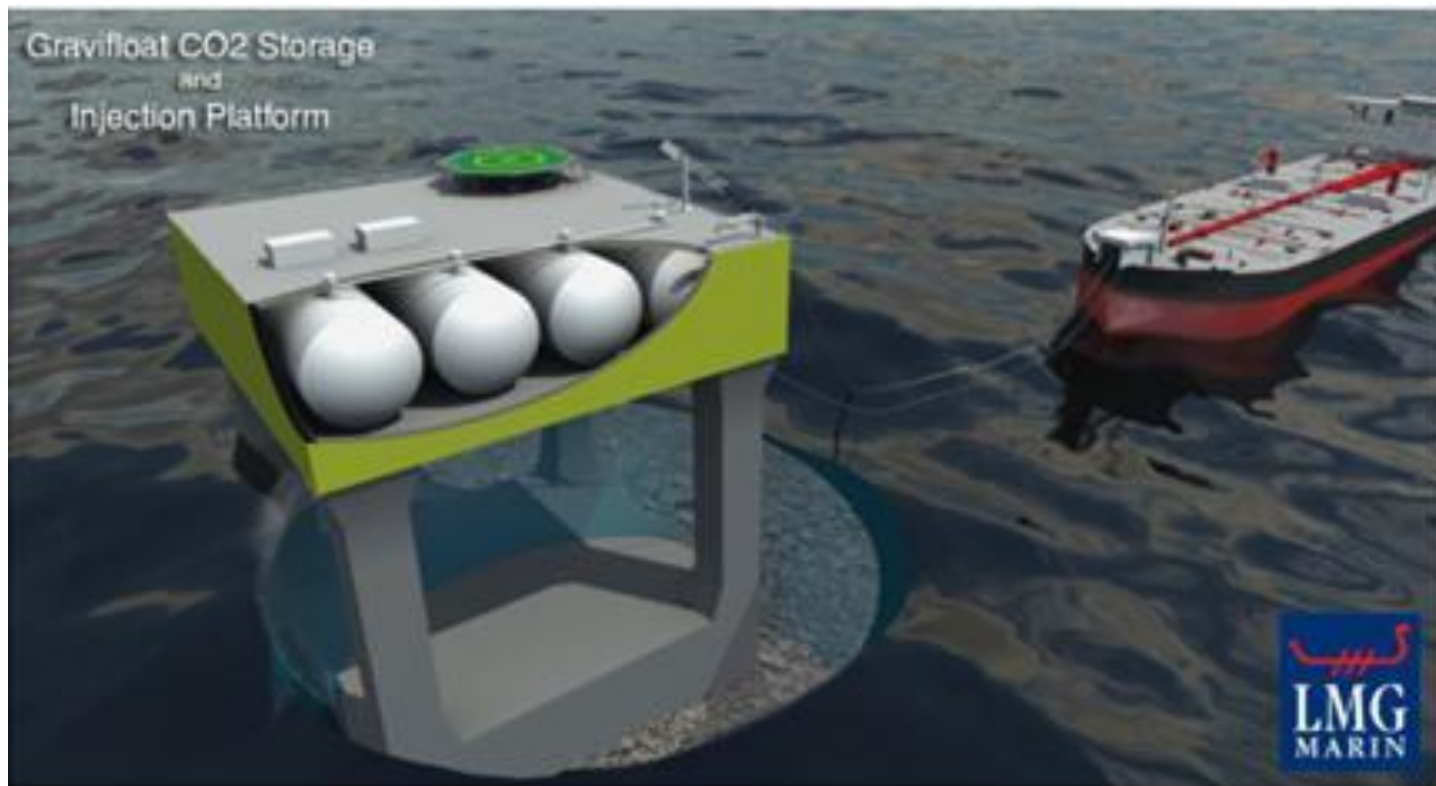
Courtesy SBM offshore

Artistic impression of a submerged turret loading (SRV2)



Courtesy APL

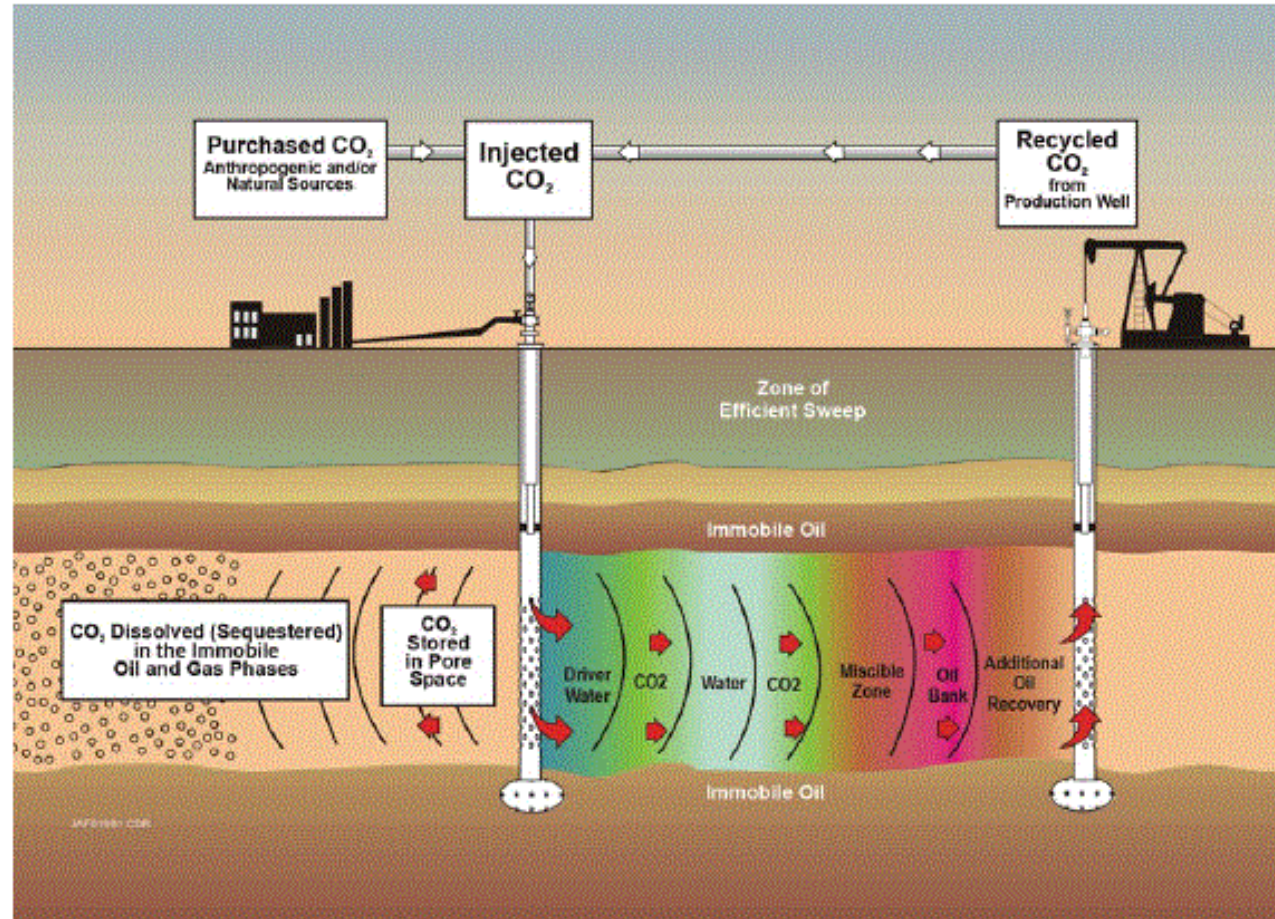
Artist's impression of a gravifloat CO₂ storage and injection platform



Water-alternating-Gas (WAG)

- › Often executed by trial-and-error
- › CO₂ EOR without storage objective
 - › CO₂ commodity
 - › Minimisation of costs of CO₂
- › CO₂ EOR with storage objective
 - › Maximisation of CO₂ storage (Carbon credits)
- › predictions combined with optimisations are required

FIGURE 66 Schematic diagram of a water-alternating-gas (WAG) miscible CO₂ EOR operation



Source: ARI and Melzer Consulting (2010).

Applied Reservoir models

- › Properties of oil as a function of CO₂ concentration
- › Based on lab tests

- › Simulator
 - › Black-oil simulator Eclipse 100
 - › (Schlumberger)

Initialisation Simulator

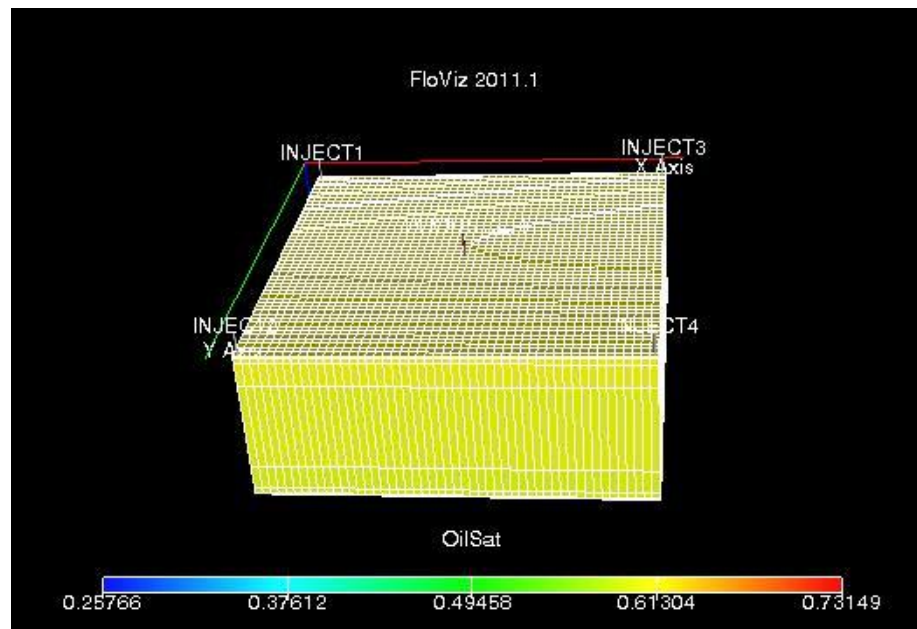
Immiscible CO₂ EOR

5 spot pilot

$P_i = 150$ Bar

Δz

1
4
16
58
16
4
1



constraints

Inject. = 165 bar

Prod.=100 bar



250 m

Medium heavy oil

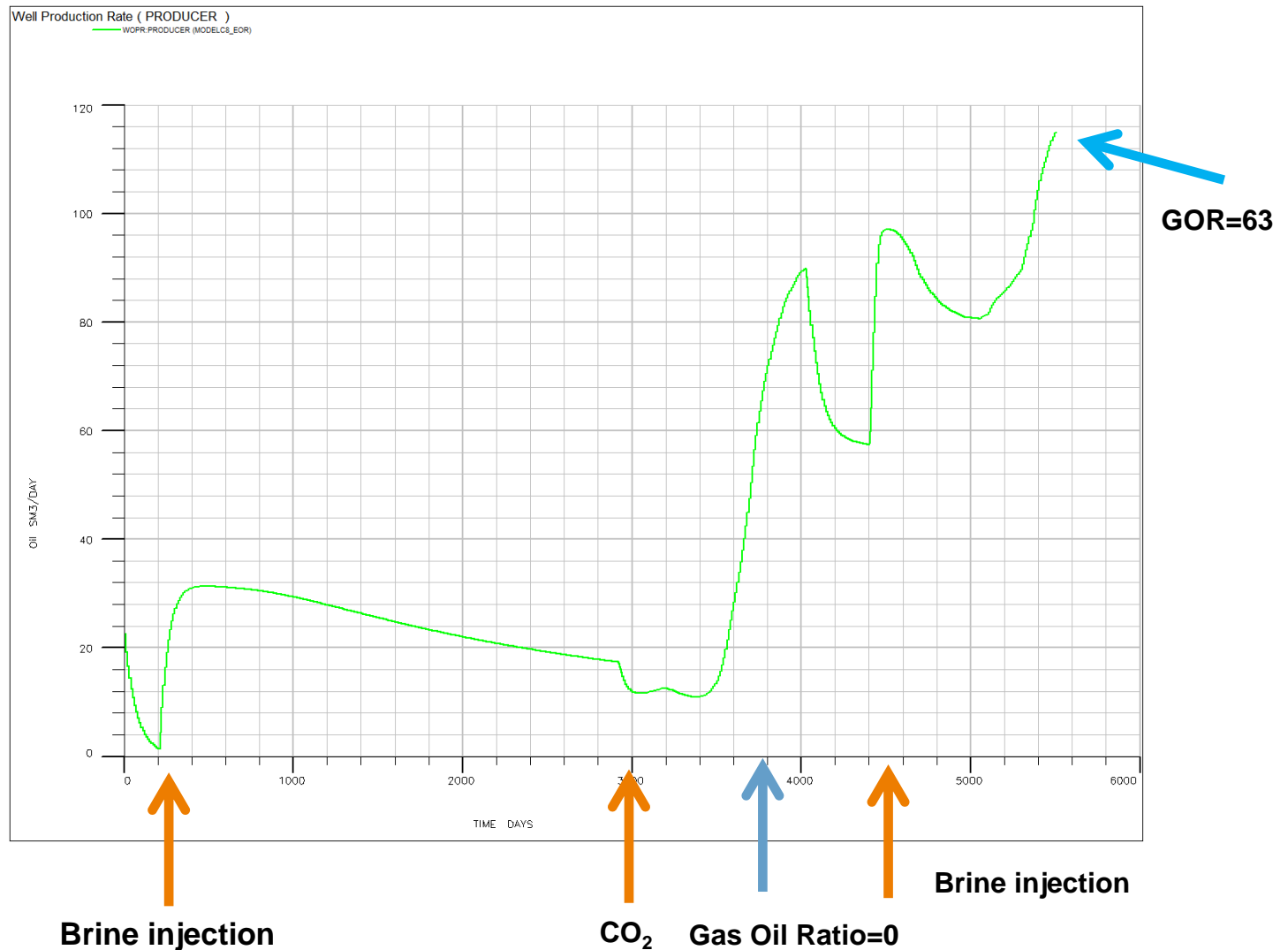
PERM = 200 mD

50*50*7 grids

kv/kh=0.1

Properties oil as function of CO₂ (SPE 107163)

Predicted oil production as function of time



Optimization of CO2 WAG

- In-house optimization tool
- Simple Net Present Value model based
 - on cost and benefits of water, CO2 and benefits of produced oil
- reservoir model and controls as before

- Results are compared against original predictions

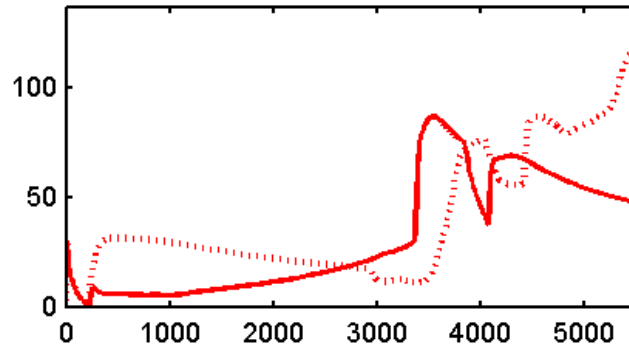
Optimisation assumptions *

- Benefits oil produced : 50 \$/bbl
- Costs of water injection: 1 \$/bbl,
- Costs of water produced: 0 \$/bbl,
- Costs of CO₂ injected: 50\$/ton
- no discounting
- 2 WAG cycles (CO₂-water)

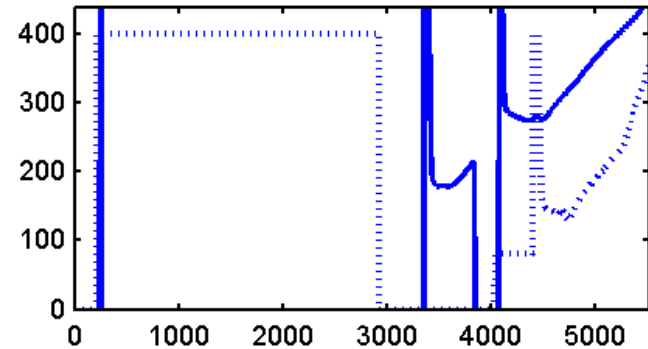
- * example only

Optimisation Example

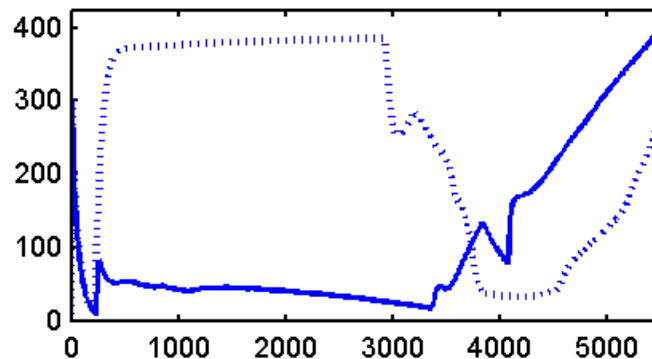
oil produced



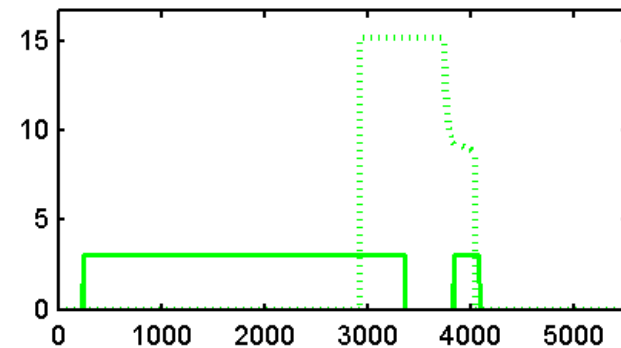
water injected



water produced



$\times 10^4$ CO2 injected



Dashed line: reference case, solid line: optimisation example

Conclusions

- › Real flow of multiple phases quite different from ideal picture as shown
- › Besides swelling and reduced viscosity, different sweeping areas between the injected water and CO₂ may also lead to higher overall sweeping efficiency and oil production
- Optimisation
 - Variable costs and benefits lead to different injection and production schemes



Prices

Marginal costs: water (injection (conditioning) and production):
CO₂ (recycling/transport/capture (ETS) correct
Rate and temperature
Energy consumption etc.

Revenues: price BBL oil (fluctuating).

Whole chain optimalization by combination of economical model and
reservoir model



Example case study: EOR applied @ existing fields in NW Europe

